## CLAIMS

Method for selective separation of each of constituents of a mixture of synthetic organic materials that are polymers and/or copolymers, in particular used, and intended to be upgraded by recycling, having a density of at least 1, in fragmented form, consisting of carrying out their separation by introducing said mixture into a dense liquid medium, which is an aqueous suspension of powder particles dispersed in an adequate amount in an aqueous phase, in order to create a density level "ds" chosen as the threshold for separation of the various fragmented synthetic organic materials to be selectively separated by type, characterised in that said separating suspension is made selective, stable and invariant with regard to density at a precision level of ±0.0005 with respect to the density threshold "ds" chosen for the selective separation:

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- a) by the size selection of powder particles having a granulometric cross-section of no more than 30  $\mu m$ , which solid powder particles thus sized are dispersed and present in an aqueous phase in a sufficient amount to reach the chosen density threshold "ds", and
- b) by the implementation of at least one means of dynamic stabilisation by creating a circulating flow of said separating suspension, which circulating flow is at most  $40~\text{m}^3/\text{h}$ .
- 2. Method according to claim 1, characterised in that said separating suspension is made selective, stable and invariant with regard to density at a precision level of ±0.0005 with respect to the density threshold "ds" chosen

for the selective separation, by the size selection of solid powder particles of which the granulometric cross-section is preferably no more than 20  $\mu m$ , and very preferably no more than 5  $\mu m$ , which solid powder particles thus sized are dispersed and present in an aqueous phase in a sufficient amount to reach the chosen density threshold "ds".

- 3. Method according to claim 1, characterised in that the powder particles are of natural origin and are chosen from 10 the group of powder mineral materials constituted by clays belonging to the families formed by the group of kaolinites, including, kaolinite, dickite, halloysite, disordered kaolinites, serpentines, the group of micas, in particular, muscovite, biotite paragonite, and 15 pyrophyllite and talc, illites and glauconite, the group of montmorillonites, in particular beidellite, stevensite, saponite and hectorite; the group of chlorites; the group of vermiculites; the group of interstratified clays of which the unitary structure is a combination of the 20 previous groups; the group of fibrous clays, in particular attapulgite (palygorskite) and sepiolite; the group formed by calcium carbonate (calcite), magnesium carbonate, dolomite (double carbonate of calcium and magnesium), calcium sulphate dihydrate (gypsum), barium sulphate, talc, 25 alumina, silica, titanium dioxide and zirconium.
- Method according to claim 1, characterised in that the powder particles are of synthetic origin and are chosen
   from the group consisting of glass powders, calcium carbonate precipitate and metallic powders.

5. Method according to at least one of claims 1 to 4, characterised in that the powder particles have a median diameter of no more than 5  $\mu m$  and preferably between 1  $\mu m$  and 0.005  $\mu m$ .

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- 6. Method according to at least one of claims 1 to 5, characterised in that the means of dynamic stabilization are selected from the group consisting of agitation by means of an agitation rotor, internal recirculation of the suspension by means of the agitation rotor, external recirculation of the suspension by means of a pump by withdrawing the suspension from the base of the container where it is located and by reinjection into the upper portion of said container, or by a combination of means enabling both the agitation by means of an agitation rotor and the internal and/or external recirculation of the suspension.
- 7. Method according to at least one of claims 1 to 6, characterised in that the means of dynamic stabilisation consist of continuous or non-continuous recirculation of the suspension.
- 8. Method according to claim 1, characterised in that the circulating flow of the separating suspension is between 5 and 30  $m^3/h$  and preferably between 5 and 15  $m^3/h$ .
  - 9. Method according to at least one of claims 1 to 8, characterised in that the circulating flow of the separating suspension is adjusted at an hourly turnover rate of said suspension between 0.5 and 4 and preferably between 0.5 and 2.

10. Method according to at least one of claims 1 to 9, characterised in that the aqueous phase has a conductivity of no more than 50 ms and preferably between 0.2 ms and 40 ms.

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- 11. Method according to at least one of claims 1 to 10, characterised in that a water-soluble agent for assisting with the stabilization of the rheological and invariance characteristics of the apparent density "ds" of the solid powder particle suspension is added to said suspension.
- 12. Method according to claim 11, characterised in that water-soluble agent for assisting with the the of the rheological stabilization and invariance characteristics of the apparent density "ds" of the solid powder particle suspension is chosen from the group phosphates and polyphosphates, consisting of alkylphosphate esters, alkylphosphonate, alkylsulphate, alkylsulfonate, lignin, lignosulfonates in the form of calcium, sodium, iron, chromium, or iron and chromium maleic anhydride and sulfonic styrene acid salts, copolymers, substituted, neutralised, esterified or nonmethylacrylamide and (methyl)acrylic acid esterified copolymers, methylacrylamide-alkyl sulfonic acid and (methyl)acrylamide copolymers, water-soluble acrylic acid polymers used in acid form or, optionally, entirely or partially neutralised by alkaline and/or alkaline-earth agents, by amines and/or salified by monovalent and/or polyvalent ions, and/or esterified, or from water-soluble acrylic copolymers having phosphatized, phosphonated, sulfated or sulfonated functions.
  - 13. Method according to either one of claims 11 and 12, characterised in that the water-soluble stabilisation

agent is preferably selected from the water-soluble acrylic copolymers, having the general formula:

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- Z is a phosphate, phosphonate, sulfate or sulfonate motif having at least one free acid function,
  - n has a value between 0 and 95,
  - p has a value between 95 and 5,
  - q has a value between 0 and 95,
  - the sum of n + p + q is equal to 100,
- $R_1$  and  $R_2$  can simultaneously be hydrogen, or while one is hydrogen, the other can be a carboxylic function esterified or not by an alcohol in  $C_1$  to  $C_{12}$ ,
  - $R_3$  can be hydrogen or an alkyl radical in  $C_1$  to  $C_{12}$ ,
- $R_4$  and  $R_5$  are, simultaneously or not, hydrogen or an alkyl radical in  $C_1$  to  $C_{12}$ , a substituted or unsubstituted aryl, a carboxylic function esterified or not by an alcohol in  $C_1$  to  $C_{12}$ ,
- $R_6$  is a radical that establishes the bond between the motif Z and the polymer chain, which radical  $R_6$  can be an alkylene of formula  $\{CH_2\}_r$  in which r can have the values in the interval 1 to 12, an alkylene oxide or polyoxide of formula  $\{R_8\longrightarrow O\}_s$  in which  $R_8$  is an alkylene in 25  $C_1$  to  $C_4$  and s can have a value from 1 to 30, or a combination of the two formulas  $\{CH_2\}_r$  and  $\{R_8\longrightarrow O\}_s$ ,
  - $R_7$  is hydrogen or an alkyl radical in  $C_1$  to  $C_{12}$ ,

- $R_9$  and  $R_{10}$  are simultaneously hydrogen, or while one is hydrogen, the other is a carboxylic grouping, an ester in  $C_1$  to  $C_{12}$ , an alkyl in  $C_1$  to  $C_{12}$ , or an alkylaryl,
- $R_{11}$  is hydrogen, a carboxylic grouping, an alkyl in  $C_1$  to  $C_3$  or a halogen,
  - $R_{12}$  is an ester in  $C_1$  to  $C_{12}$ , a substituted or unsubstituted amide, an alkyl in  $C_1$  to  $C_{12}$ , an aryl in  $C_5$  or  $C_6$ , an alkylaryl, a halogen, a carboxylic grouping or a phosphatized, phosphorated, sulfated or sulfonated alkyl or aryl grouping.
  - 14. Method according to claim 13, characterised in that the motif Z, the non-free acid functions are occupied by a cation, an ammonium grouping, an amine, an alkyl in  $C_1$  to  $C_3$ , a substituted or an unsubstituted aryl in  $C_3$  to  $C_6$ , an alkylaryl, an ester in  $C_1$  to  $C_{12}$ , preferably in  $C_1$  to  $C_3$ , or a substituted amide.
- 15. Method according to claim 13, characterised in that in the sum of n + p + q, n = 0, when q > 0, and q = 0 when n > 0.
- 16. Method according to claim 13, characterised in that, in the motifs  $R_1$  and  $R_2$ , the alcohol esterifying the carboxylic function is preferably in  $C_1$  to  $C_4$ .
  - 17. Method according to claim 13, characterised in that, in the motif  $R_3$ , the alkyl radical is preferably in  $C_1$  to  $C_4$ .

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18. Method according to claim 13, characterised in that, in the motifs  $R_4$  and  $R_5$ , the alkyl radical is preferably in  $C_1$  to  $C_4$ .

- 19. Method according to claim 13, characterised in that, in the motifs  $R_4$  and  $R_5$ , the alcohol esterifying the carboxylic function is preferably in  $C_1$  to  $C_4$ .
- 5 20. Method according to claim 13, characterised in that, in the motif  $R_7$ , the alkyl radical is preferably in  $C_1$  to  $C_4$ .
- 21. Method according to claim 13, characterised in that, in the motifs  $R_9$  and  $R_{10}$ , the ester is preferably in  $C_1$  to  $C_3$ .
- 22. Method according to claim 13, characterised in that, in the motifs  $R_9$  and  $R_{10}$ , the alkyl is preferably in  $C_1$  to  $C_3$ .
  - 23. Method according to claim 13, characterised in that, in the motif  $R_{12}$ , the ester is preferably in  $C_1$  to  $C_5$ .
- 20 24. Method according to claim 13, characterised in that, in the motif  $R_{12}$ , the alkyl is preferably in  $C_1$  to  $C_3$ .
- 25. Method according to claim 13, characterised in that the molecular weight of the water-soluble acrylic copolymers forming the stabilisation agent is between 5000 and 100,000.
- 26. Method according to claim 13, characterised in that the water-soluble acrylic copolymers forming the stabilisation agent are at least partially neutralised, by means of a neutralisation agent chosen from the group consisting of sodium, potassium, ammonium, calcium and magnesium hydroxides, and primary, secondary and tertiary amines, aliphatic and/or cyclic, in particular mono-, di-

and tri-ethanolamines, mono- and diethylamines, cyclohexylamine and methylcyclohexylamine.

27. Method according to any one of claims 10 to 13, characterised in that the weight of the water-soluble stabilisation agent, expressed as a dry/dry weight percent of said agent with respect to the weight of the powder particles in suspension, is between 0.02 % and 5 %, and preferably between 0.1 % and 2 %.

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28. Method according to at least one of claims 1 to 27, characterised in that said method is performed in at least one hydraulic separator equipped with at least one dynamic stabilisation means.

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- 29. Method according to claim 28, characterised in that, when said method is performed in a single hydraulic separator, the chosen density "ds" changes:
- in the increasing direction, by a controlled 20 addition of predefined and selected powder particles to the suspension present in the hydraulic separator, until the new chosen threshold density "ds" is reached,
  - in the decreasing direction, by adding water until the new chosen threshold density "ds" is reached.

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30. Method according to claim 29, characterised in that the change in density of the stable separating suspension, in an increasing or decreasing direction, is carried out under agitation by means of an agitation rotor and/or internal recirculation of the aqueous medium and/or recirculation of the dense medium by withdrawing the dense aqueous medium from the base of the hydraulic separator and reinjecting it into the top portion of said separator of the dense aqueous medium being adjusted.

31. Method according to claim 28, characterised in that, if said method is performed in a plurality of hydraulic separators, the various separators are placed one after another, in a cascade system functioning with stable suspensions each having a specific density threshold "ds", in an increasing or decreasing order of density.

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- 32. Method according to any one of claims 28 to 31, characterised in that the threshold density "ds" of the aqueous suspension for fine separation is continuously controlled by appropriate measurement means and subjected to an adjustment when any deviation is detected.
- 33. Method according to claim 32, characterised in that each hydraulic separator is controlled with regard to the 15 density of the dense medium that it contains by means of two electrical valves each opening onto two circuits connected to two tanks, one of the tanks containing a "mother" suspension with a concentration of around 60 % stabilised powder particles, by water-soluble a 20 stabilizing agent, enabling a predetermined amount of the mother suspension to be added, which adjusts upward any deviation toward a reduction in the density of the dense medium for fine separation, and the other tank containing water enabling a predetermined amount to be added so as to 25 adjust downward any deviation toward in increase in the density of the dense medium for fine separation.
- 34. Method according to claim 33, characterised in that,
  30 in each hydraulic separator, the measurement of the
  density of the dense medium is performed continuously by
  suitable measuring apparatuses that activate the opening
  of one or the other of the electrical valves, then the

closing thereof when the threshold density level "ds" is reached.

35. Use of the method according to at least one of claims
5 1 to 34 for the selective separation of a mixture of
polymer materials, in particular used, from the
destruction of automobiles and/or durable consumer goods
that have reached the end of their serviceable lives.